



## CHAOS IN A HYDRAULIC CONTROL VALVE

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In this paper we have studied the instability and chaos occurring in a pilot-type poppet valve circuit. The system consists of a poppet valve, an upstream plenum chamber, a supply pipeline and an orifice inserted between the plenum and the pipeline. Although the poppet valve rests on the seat stably for a supply pressure lower than the cracking pressure, the circuit becomes unstable for an initial disturbance beyond a critical value and develops a self-excited vibration. In this unstable region, chaotic vibration appears at the period-doubling bifurcation. We have investigated the stability of the circuit and the chaotic phenomenon numerically, and elucidated it by power spectra, a bifurcation diagram and Lyapunov exponent calculations, showing that the phenomenon follows the Feigenbaum route to chaos.

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### 1. INTRODUCTION

POPPET valves are pressure-regulating valves extensively used in hydraulic circuits. The circuits including the valve are classified into two categories: a direct-acting type and a pilot type. In the former the poppet valve is directly connected to a pipeline, while in the latter the valve is connected to a pipeline through an orifice and a plenum chamber. Both types of poppet valve circuits often become unstable, developing self-excited vibrations and often exhibiting irregular (chaotic) behaviour during self-excitation (Hayashi 1995).

The vibratory modes of the circuit consist of a poppet valve mode and an infinite number of pipeline modes corresponding to the natural frequencies of the fluid column in the connecting pipeline, infinite because of the continuous nature of the pipeline. Thus, the dynamical behaviour of the system including the poppet valve is complex.

There have been many studies on the stability of the poppet valve circuit (Backé & Rünnerburger 1964; Funk 1964; Kasai 1968a,b). However, these studies have mainly treated local stability of the system, i.e., stability of the steady static points (fixed points). Little work has been done on global stability, self-excited vibrations and chaotic phenomena in this system.

One of the authors has indicated in a previous study that various kinds of chaotic vibrations occur in a direct-acting poppet valve circuit with a long lossless pipeline (Hayashi & Mochizuki 1987; 1989). In that study, it was found that the pipeline mode vibrations become unstable in turn starting from low frequency modes with increasing pipeline length. The system was found to have multiple unstable modes for a long pipeline. As a result, the system exhibits diverse self-excited vibrations, including period-doubling, almost periodic vibration composed of two unstable modes of vibration, phase-locking phenomena between two unstable modes, and chaotic vibration.

Using numerical simulation and experiments, the possibility of Feigenbaum-type chaos was shown for a relatively short pipeline circuit and Lorenz-type chaos and intermittent-type chaos for a long pipeline circuit.

Similarly to the direct-acting poppet valve, chaotic vibration is expected to occur in a pilot-type poppet valve circuit. Hayashi & Ohi (1993) performed numerical analysis for the case with a short supply pipeline. It was found that, even when the valve stably rests on the valve seat for a supply pressure lower than the cracking pressure, self-excited vibration occurs if a disturbance larger than a critical value is given to the poppet valve. This means the system undergoes subcritical instability. Occurrence of the chaotic vibration, however, has still not been confirmed in this self-excited vibration regime.

In the present study, the authors perform detailed numerical analysis on the chaotic vibration occurring in a pilot-type poppet valve circuit with a short pipeline. The dynamics can be approximated by a lumped parameter model. The numerical analysis shows that the resulting self-excited vibration undergoes transition, changing from a period-one vibration to a chaotic vibration through a period-doubling bifurcation cascade, with the supply pressure as a system parameter.

## 2. GOVERNING EQUATIONS

Figure 1 is a schematic diagram of a pilot-type poppet valve circuit considered here. The valve function is to keep the circuit pressure constant in case of excess flow in hydraulic systems. The working fluid flows from a constant pressure supply tank, passes through a pipeline, an orifice and a valve chamber, and flows out to the atmosphere from the poppet valve when the supply pressure exceeds the 'cracking' pressure  $P_{Si}$ , which is pre-adjusted by the spring supporting the poppet valve.

Governing equations describing the behaviour of the system are derived referring to Figure 1. The equation of motion of the poppet is described as a vibratory system with a single degree of freedom; thus,

$$m \frac{d^2 X}{dt^2} + \delta \frac{dX}{dt} + kX + f_0 = F, \quad (1)$$

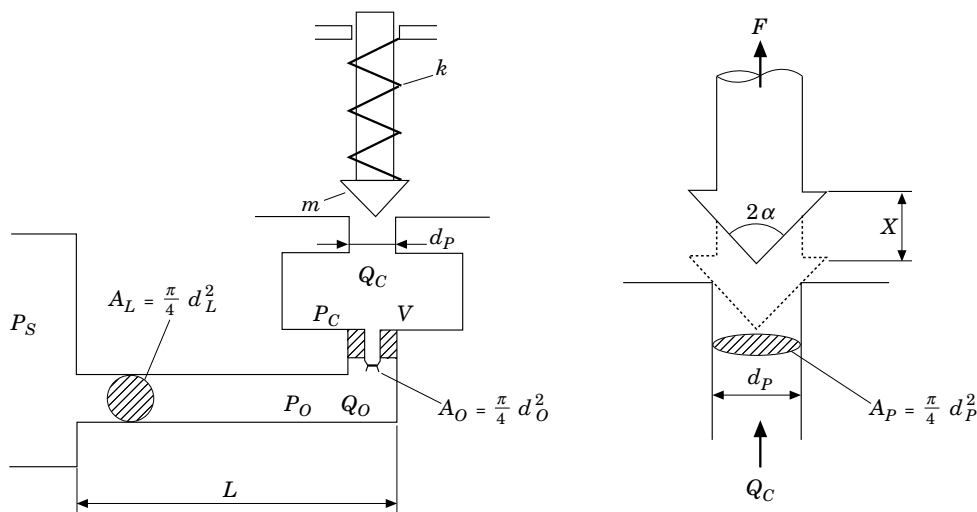


Figure 1. Schematic diagram of a poppet valve circuit of pilot type.

where  $X$  is the valve displacement (valve lift),  $m$  the mass of the poppet,  $\delta$  the viscous damping coefficient,  $k$  the stiffness of the spring supporting the poppet, and  $f_0$  the initial spring compression force.  $f_0$  may be varied in order to pre-adjust the cracking pressure  $P_{Si}$  at which the valve begins to open, according to

$$f_0 = kX_i = A_p P_{Si}, \quad (2)$$

where  $X_i$  is the initial spring compression and  $A_p$  the cross-sectional area of the valve-seat aperture.  $F$  is the axial flow force acting on the poppet. For a sharp-edged valve seat, this axial force is given by (Takenaka & Urata 1975)

$$F = A_p P_C [1 - 4C_p (X/d_p) \sin 2\alpha], \quad (3)$$

where  $P_C$  is the valve chamber pressure,  $C_p$  the discharge coefficient of the poppet valve [see equation (7) below],  $d_p$  the diameter of the valve-seat aperture, and  $\alpha$  the half-angle of the poppet.

The capacitive characteristic of the valve chamber is described by

$$\frac{V dP_C}{\beta dt} = Q_O - Q_C, \quad (4)$$

where  $Q_O$  is the orifice flow rate,  $Q_C$  the poppet valve flow rate,  $V$  the valve chamber volume, and  $\beta$  the bulk modulus of the working fluid.

Since the supply line length is assumed to be short ( $L = 0.3$  m), the dynamics of the pipeline can be approximated by the lumped parameter model

$$\frac{\rho L dQ_O}{A_L dt} = P_S - P_O, \quad (5)$$

where  $P_S$  is the supply pressure,  $L$  the length of the pipeline and  $A_L$  the cross-sectional area of the pipeline.

The flow rate through the poppet valve is

$$Q_C = C_p \pi d_p X \sin \alpha \sqrt{\frac{2\Psi(P_C)}{\rho}}, \quad (6)$$

where  $d_p$  is the diameter of the valve seat,  $\rho$  is the density of the working fluid, and  $C_p$  is the discharge coefficient of the poppet valve, which changes almost linearly for small valve lift and becomes constant for large valve lift. Thus, it is approximated on the basis of the experimental results shown in Figure 2 by the following formula:

$$C_p = C_{p0} \left( \frac{\gamma X}{1 + \gamma X} \right), \quad (7)$$

where  $C_{p0} = 0.8$  and  $\gamma = 40\,000 \text{ m}^{-1}$ .  $\Psi(P_C)$  is a function defined as follows:

$$\Psi(P_C) = \begin{cases} P_C & \text{for } P_C > 0 \\ 0 & \text{for } P_C < 0. \end{cases} \quad (8)$$

When the pressure in the valve chamber drops below atmospheric pressure in the actual system, air dissolved in the working fluid is released and forms a cavity. As a result, the chamber pressure is maintained at atmospheric pressure.  $\Psi(P_C)$  in equation (6) simulates this actual situation.

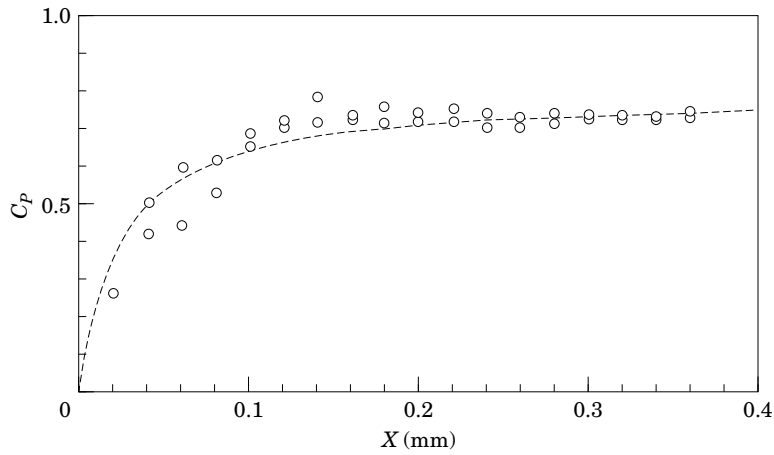


Figure 2. Experimental result for discharge coefficient of poppet valve ( $d_p = 6$  mm,  $P_{S_i} = 4$  MPa): (---)  $C_p = 0.8\gamma X/(1 + \gamma X)$ ; (O), experimental.

The orifice flow  $Q_O$  is

$$Q_O = C_O A_O \operatorname{sgn}(P_O - P_C) \sqrt{\frac{2|P_O - P_C|}{\rho}}, \quad (9)$$

where  $C_O$  is the discharge coefficient of the orifice and  $A_O$  the area of the orifice.

The vibrating poppet sometimes impacts against the valve seat. In particular, this inevitably occurs for supply pressures below the cracking pressure. The following collision condition is applied in the numerical simulation

$$\dot{X}(t^+) = -e\dot{X}(t^-), \quad X(t^\pm) = 0, \quad (10)$$

where  $\dot{X}(t^-)$  and  $\dot{X}(t^+)$  are the valve velocities just before and after collision, respectively, and  $e$  is the restitution coefficient.

To recapitulate, the set of governing equations may be summarized as follows:

$$\begin{aligned} m\ddot{X} + \delta\dot{X} + k(X + X_i) &= A_p P_C \left[ 1 - 4C_{p0} \left( \frac{\gamma X^2}{1 + \gamma X} \right) \frac{1}{d_p} \sin 2\alpha \right], \\ \dot{P}_C &= \left( \frac{\beta}{V} \right) \left[ Q_O - C_{p0} \left( \frac{\gamma X^2}{1 + \gamma X} \right) \pi d_p \sin \alpha \sqrt{\frac{2\Psi(P_C)}{\rho}} \right], \\ \dot{Q}_O &= \left( \frac{A_L}{\rho L} \right) \left[ P_S - P_C - \frac{\rho}{2C_O^2 A_O^2} |Q_O| Q_O \right], \\ \dot{X}(t^+) &= -e\dot{X}(t^-), \quad X(t^\pm) = 0. \end{aligned} \quad (11)$$

The nonlinear simultaneous equations (11) for the unknown variables  $X$ ,  $P_C$  and  $Q_O$  are numerically solved by the Runge–Kutta (R–K) method. The calculation is mainly carried out for a supply pressure lower than the cracking pressure of the valve; thus, the poppet inevitably collides against the valve seat, as stated previously. In general, the collision occurs in the interval of meshpoints of time in the numerical calculation. The total accuracy of the numerical solution is markedly reduced, if the collision time instant is calculated by the ordinary, simple linear interpolation; if  $X(t_n)X(t_{n+1}) < 0$ , then the instant of collision is given as  $[X(t_{n+1})t_n - X(t_n)t_{n+1}]/[X(t_{n+1}) - X(t_n)]$ . The calculation here is performed by using the “time stepsize subdivision method”

TABLE 1  
System parameters used in simulation

Quantity	Symbol	Value	Units
Discharge coefficient of orifice	$C_O$	0.64	
Valve diameter	$d_P$	$6.0 \times 10^{-3}$	m
Orifice diameter	$d_O$	$2.0 \times 10^{-3}$	m
Pipeline diameter	$d_L$	$8.9 \times 10^{-3}$	m
Restitution coefficient	$e$	0.65	
Spring stiffness	$k$	$1.284 \times 10^4$	N/m
Pipeline length	$L$	0.3	m
Valve mass	$m$	$7.4 \times 10^{-2}$	kg
Valve chamber volume	$V$	$8.1 \times 10^{-6}$	m <sup>3</sup>
Half angle of poppet	$\alpha$	45	deg
Bulk modulus	$\beta$	$1.484 \times 10^9$	N/m <sup>2</sup>
Damping coefficient	$\delta$	4.905	kg/s
Density of fluid	$\rho$	$8.563 \times 10^2$	kg/m <sup>3</sup>

proposed by one of the authors (Hayashi, Iizuka & Hayase 1994a), which makes the accuracy of calculation for the collision instant to match that of the R-K method, by iteratively reducing the time step-size between two nodal points of time  $t_n$  and  $t_{n+1}$  containing a collision point.

The system parameters used in the simulation are listed in Table 1.

To perform the computations, the Cray Y-MP/8 in the Institute of Fluid Science, Tohoku University was used. This computer has 16 significant digits in decimal numeration for single precision arithmetic. The time step-size used was  $h = 1.0 \times 10^{-7}$  s. The highest frequency of the self-excited vibration considered here is about  $f_n \approx 1050$  Hz, as seen from the power spectra to be shown later, so the dimensionless time step-size is  $H = f_n h = 1.05 \times 10^{-4}$ . Considering that a rough indication of the accumulated error of the R-K method is of the order of  $h^4$ , the total accuracy of the calculation is satisfactory.

### 3. LOCAL STABILITY

As a starting point for the analysis, a study of the local system stability is performed. To facilitate this, equations (11) are linearized at a static state ( $X_E, P_{CE}$  and  $Q_{OE}$ ) to the following form:

$$\begin{aligned}
 m\ddot{x} + \delta\dot{x} + kx &= a_P p_c - k_X x, \\
 \dot{p}_c &= \left(\frac{1}{C}\right)(q_O - c_P p_c - c_X x), \\
 \dot{q}_O &= -\left(\frac{1}{I}\right)\left(p_c + \frac{1}{C_O} q_O\right), \\
 C &= \frac{V}{\beta}, \quad I = \frac{\rho L}{A_L}, \quad a_P = \left(\frac{\partial F}{\partial P_C}\right)_E, \quad k_X = -\left(\frac{\partial F}{\partial X}\right)_E, \\
 c_P &= \left(\frac{\partial Q_C}{\partial P_C}\right)_E, \quad c_X = \left(\frac{\partial Q_C}{\partial X}\right)_E, \quad c_O = \frac{C_O^2 A_O^2}{\rho Q_{OE}},
 \end{aligned} \tag{12}$$

where the variables  $x, p_c$  and  $q_O$  represent variational quantities from static state

values  $A_E$ ,  $P_{CE}$  and  $Q_{OE}$ , in which the subscript E indicates the values at the steady static state, which are obtained for the given  $P_{Si}$  ( $=kX_i/A_P$ ) and  $P_S$  from the following equations:

$$\begin{aligned} k(X + X_i) &= A_P P_C \left[ 1 - 4C_{P0} \left( \frac{\gamma X^2}{1 + \gamma X} \right) \frac{1}{d_P} \sin 2\alpha \right], \\ Q_O - C_{PO} \left( \frac{\gamma X^2}{1 + \gamma X} \right) \pi d_P \sin \alpha \sqrt{\frac{2P_C}{\rho}} &= 0, \\ P_S - P_C - \frac{\rho}{2C_O^2 A_O^2} Q_O^2 &= 0. \end{aligned} \quad (13)$$

The characteristic equation is derived from equation (12), i.e.,

$$s^4 + A_3 s^3 + A_2 s^2 + A_1 s + A_0 = 0, \quad (14)$$

where

$$\begin{aligned} \omega_P^2 &= \frac{k + k_X}{m}, & \omega_L^2 &= \frac{1 + c_P/c_O}{CI}, \\ 2\zeta_P \omega_P &= \frac{\delta}{m}, & 2\zeta_L \omega_L &= \frac{c_P}{C} + \frac{1}{CI}, \\ A_0 &= \omega_P^2 \omega_L^2 + \left( \frac{a_P}{m} \right) \omega_L^2 \frac{c_X}{c_O + c_P}, \\ A_1 &= 2\zeta_P \omega_P \omega_L^2 + 2\zeta_L \omega_L \omega_P^2 + \frac{a_P c_X}{mC}, \\ A_2 &= \omega_P^2 + \omega_L^2 + (2\zeta_P \omega_P)(2\zeta_L \omega_L), \\ A_3 &= 2\zeta_P \omega_P + 2\zeta_L \omega_L. \end{aligned} \quad (15)$$

The stability condition is given as

$$A_1 A_2 A_3 - A_1^2 - A_0 A_3 > 0. \quad (16)$$

Since this system has a small damping coefficient and a small pipeline resistance, all characteristic roots are obtained as complex conjugate pairs. Therefore, the unstable modes are always dynamically unstable.

Figure 3(a) shows the stability map of the poppet valve circuit calculated from equation (16) for the static valve lift  $X_E$  and the supply pressure  $P_S$ . It is noted that the static valve lift  $X_E$  is determined from equation (13) by specifying the supply pressure  $P_S$  and the cracking pressure  $P_{Si}$ . The solid line shows the critical curve below which the system is unstable. A dashed line shows the static characteristic of the valve lift  $X$  with the supply pressure  $P_S$  corresponding to the cracking pressure  $P_{Si} = 4.0$  MPa. The static valve lift moves along the abscissa for the supply pressure smaller than  $P_{Si}$ . However, it moves along the dashed curve when the supply pressure becomes larger than  $P_{Si}$ . The static state becomes unstable on the segments AB and CD of the curve. Figure 3(b) indicates a partially enlarged stability map for the small lift region of Figure 3(a) (the ordinate is scaled to  $\sqrt{X_E}$ ). According to Figure 3(b), the valve is stable in the small lift region, including  $X = 0$ .

Figure 4 indicates the change of the natural frequencies (dotted lines) corresponding to the imaginary part of characteristic roots of the linearized system and the frequencies of self-excited vibrations obtained from the simulation (symbols  $\circ$  and

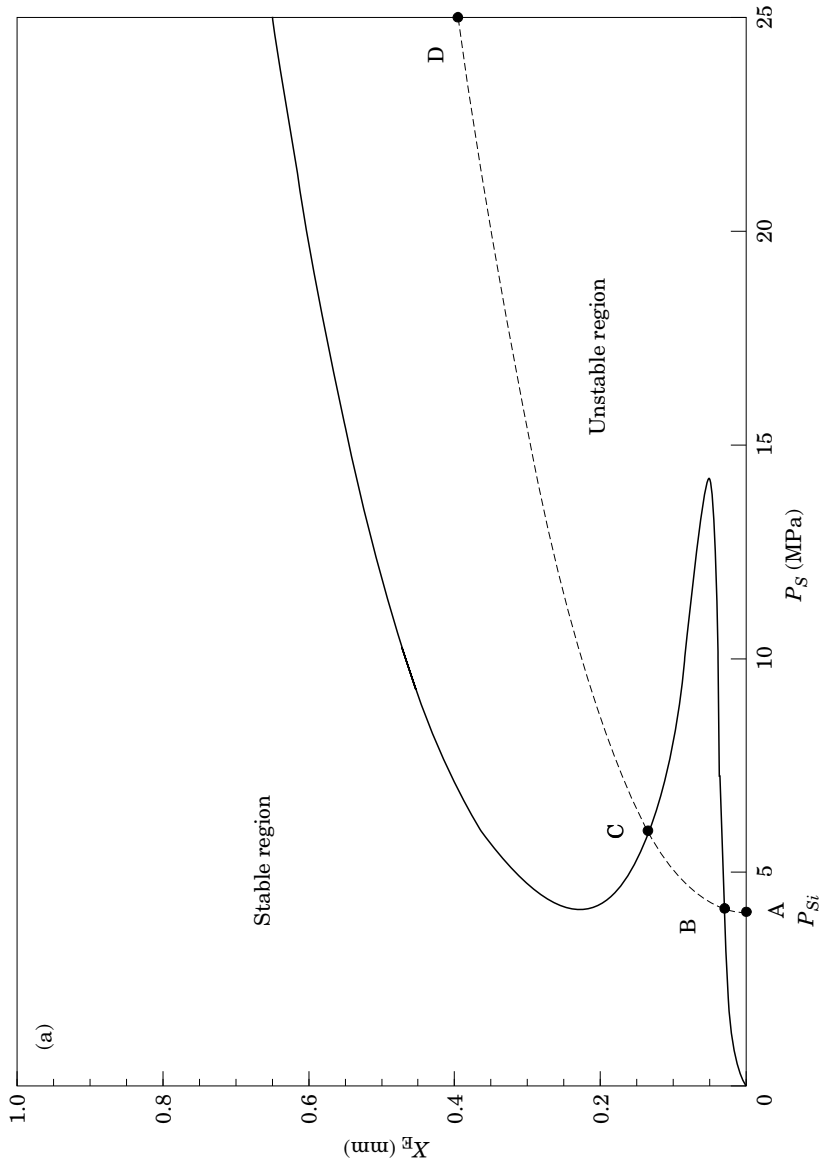


Figure 3. Stability map and steady valve lift with supply pressure: (a) Stability map over a wide area; (b) partly enlarged stability map; (---)  $P_{St} = 4.0$  MPa.

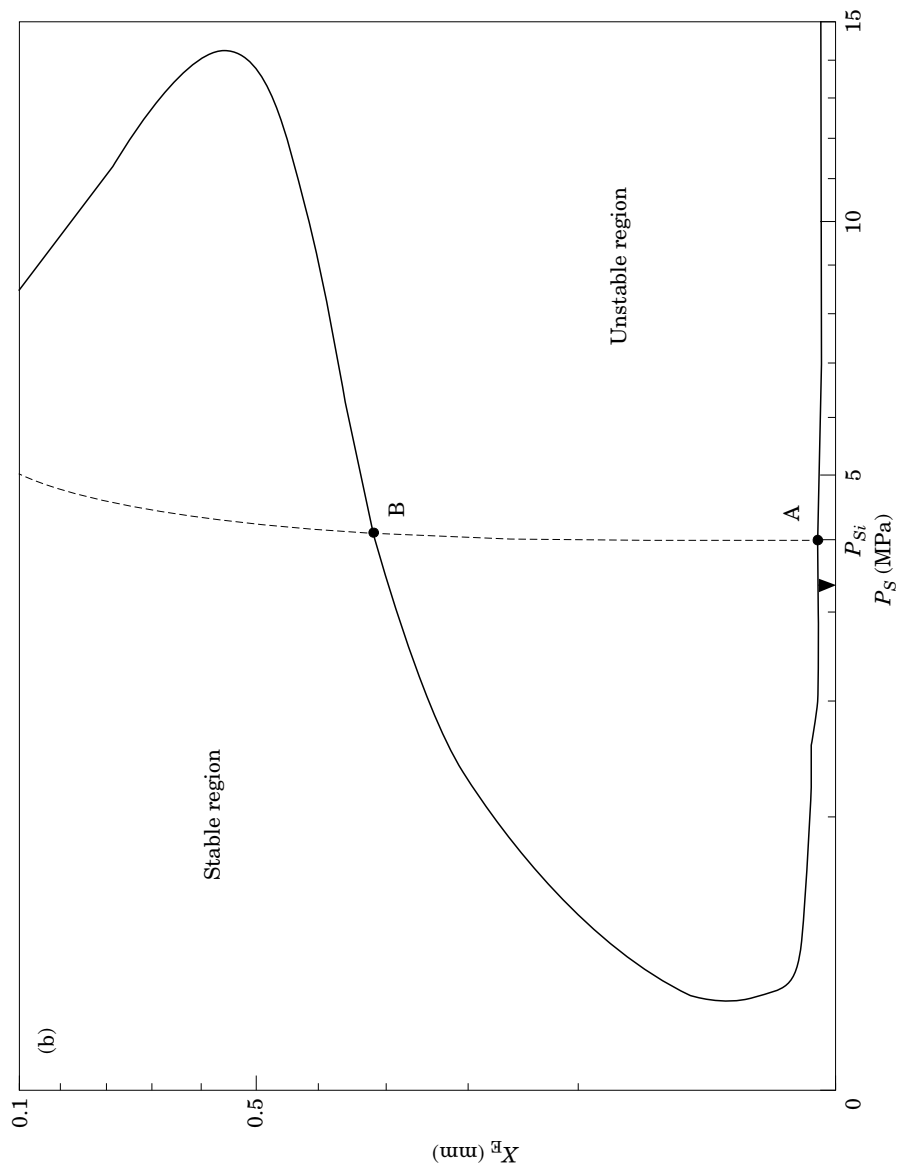


Figure 3. (Continued.)



●, respectively) with the supply pressure  $P_S$ . The natural frequencies of the linearized system at  $P_S = P_{Si}$  (cracking pressure) coincide with those of the poppet valve and the pipeline-chamber system,

$$f_p = \frac{1}{2\pi} \sqrt{\frac{k}{m}}, \quad \text{and} \quad f_L = \frac{1}{2\pi} \sqrt{\frac{\beta A_L}{\rho V L}}, \quad (17)$$

respectively. Thus, we label the corresponding vibratory modes as the ‘valve mode’ and the ‘pipeline mode’, respectively. As seen from Figure 4, the pipeline mode is unstable on the segment AB and the valve mode on the segment CD (Hayashi, Hayase & Kurahashi 1994b).

Figure 4 shows that the self-excitation of the pipeline mode occurs even for a supply pressure lower than the cracking pressure  $P_{Si}$ . This implies that it is possible for self-excited vibration to occur due to large disturbances beyond a critical value, although the poppet in steady state rests on the valve seat stably, as seen in Figure 3(b); in other words, the instability is subcritical.

The situation is demonstrated in Figure 5, which shows the responses for slightly different initial velocities, for the system having an identical operating condition which is indicated by the symbol (▼) in Figure 3(b). For the smaller initial velocity in Figure 5(a), the poppet settles down to the original steady static state and rests on the seat again, while self-excited vibration develops as shown in Figure 5(b) for a slightly larger initial velocity. This is typical of hard self-excited vibration, i.e. of subcritical instability (Hayashi & Ohi 1988, 1993). This is conjectured to be caused by a shift of the equivalent static state into the unstable region shown in Figure 3(b); the centre of the poppet positional vibration in the pipeline mode is located at some distance from the valve seat due to the collision of the poppet against the seat. Chaotic phenomena occur in this region, accompanying the hard self-excited vibration.

#### 4. CHAOTIC VIBRATION

A steady static point on the segment AB in Figure 3 is unstable, and a self-excited vibration in the pipeline mode is excited from infinitesimal disturbances. This type of vibration is so-called “soft self-excited vibration”. Once the vibration is self-excited, the vibration does not cease by lowering the supply pressure to below the cracking pressure, and the nature of the vibration shifts from soft self-excitation to the hard one. The vibration is maintained up to the considerably lower supply pressure of  $P_S = 2.8$  MPa, as seen in Figure 4.

##### 4.1. VIBRATORY WAVEFORMS, POWER SPECTRA AND PHASE PLANE PATH

A change of vibratory waveform was examined numerically under the condition that the supply pressure was increased quasi-steadily from 3.0 MPa to 4.0 MPa. In the simulation, each calculation for a given supply pressure was performed until  $t = 0.25$  s in order to allow the system to attain a steady state vibration. The supply pressure  $P_S$ , which is the system parameter varied, was then slightly increased and, for the next step of the calculation, the last set of state variables were used as initial conditions.

The results are shown in Figure 6(a)–6(f). In each case, the uppermost figure shows the displacement  $X$  of the poppet, the centre figure the power spectrum of  $X/X_{\text{ref}}$  (the reference quantity  $X_{\text{ref}} = 1$  m) and the bottom figure the phase-plane plot of  $X$  vs.  $\dot{X}$ .

In Figure 6(a) for  $P_S = 3.4$  MPa, the waveform of the vibration is almost sinusoidal with a frequency corresponding to the pipeline mode frequency. In Figure 6(b), for

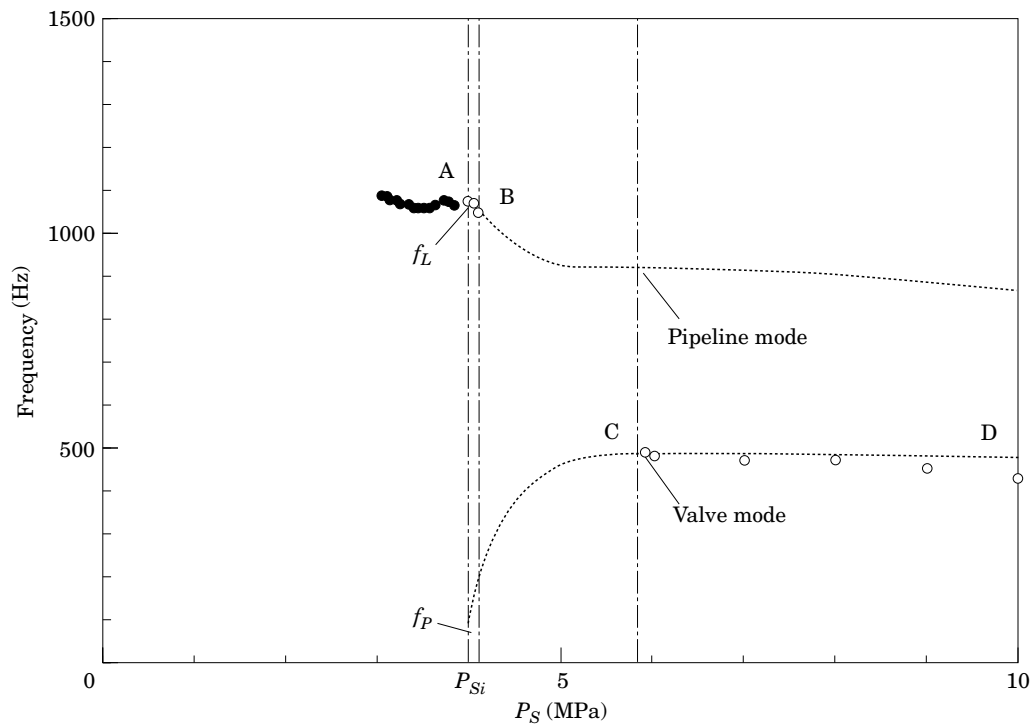


Figure 4. Natural frequencies of the system ( $P_{Si} = 4.0$  MPa): (●), hard self-excitation; (○), soft self-excitation.

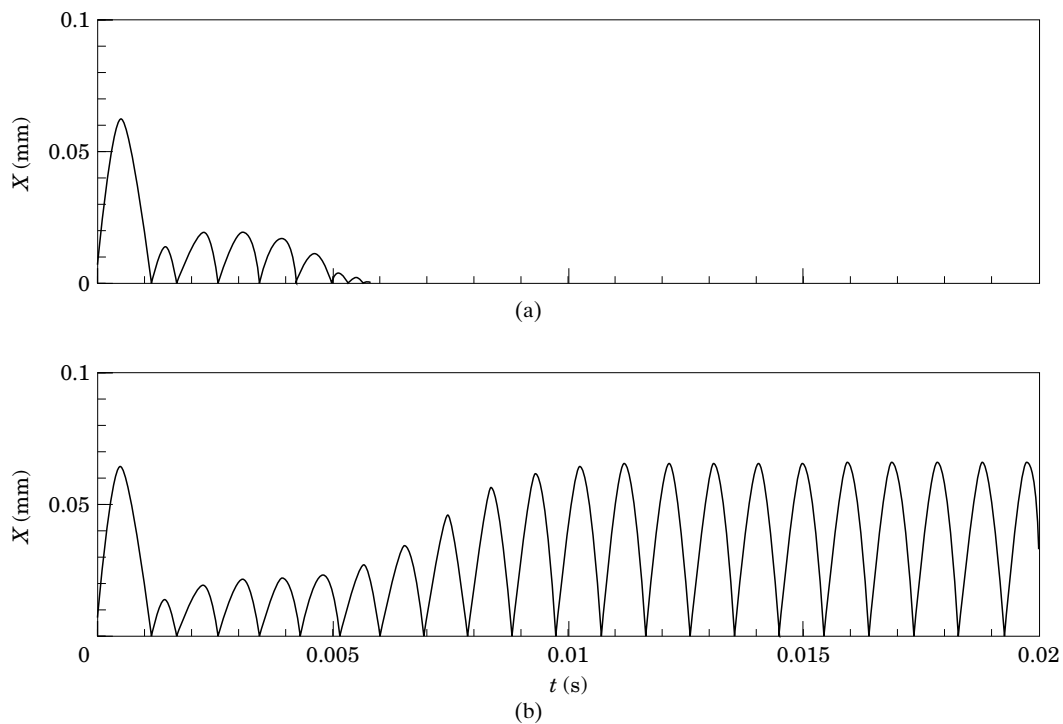


Figure 5. Responses of poppet valve for slightly different initial conditions: (a) initial velocity  $\dot{X}(0) = 0.212$  m/s, supply pressure  $P_S = 3.4$  MPa; (b)  $\dot{X}(0) = 0.215$  m/s,  $P_S = 3.4$  MPa.

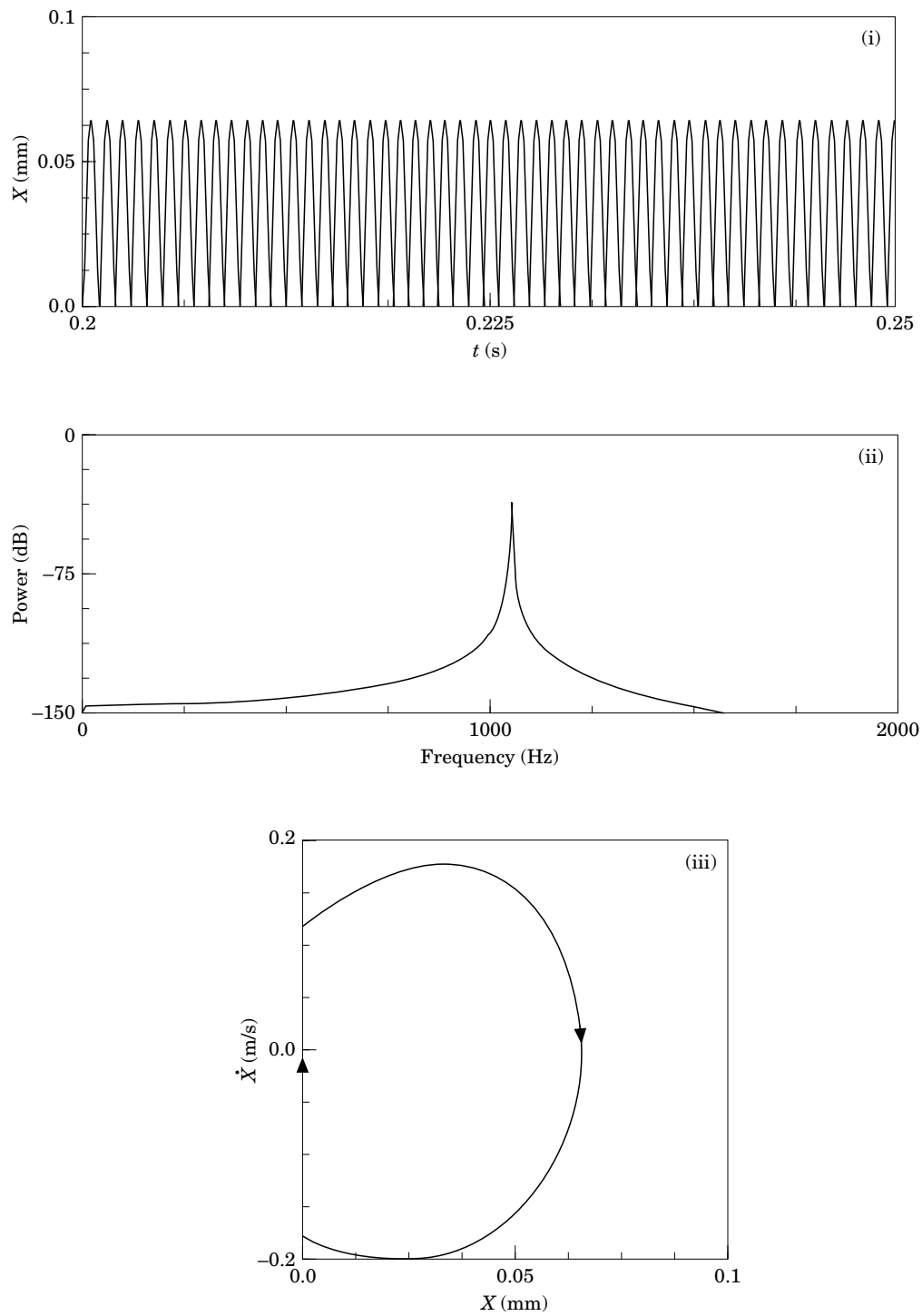


Figure 6(a). Comparison of self-excited vibrations in different supply pressure for  $P_s = 3.4$  MPa; period-one vibration: (i) poppet vibration; (ii) power spectrum; (iii) phase-plane plot.

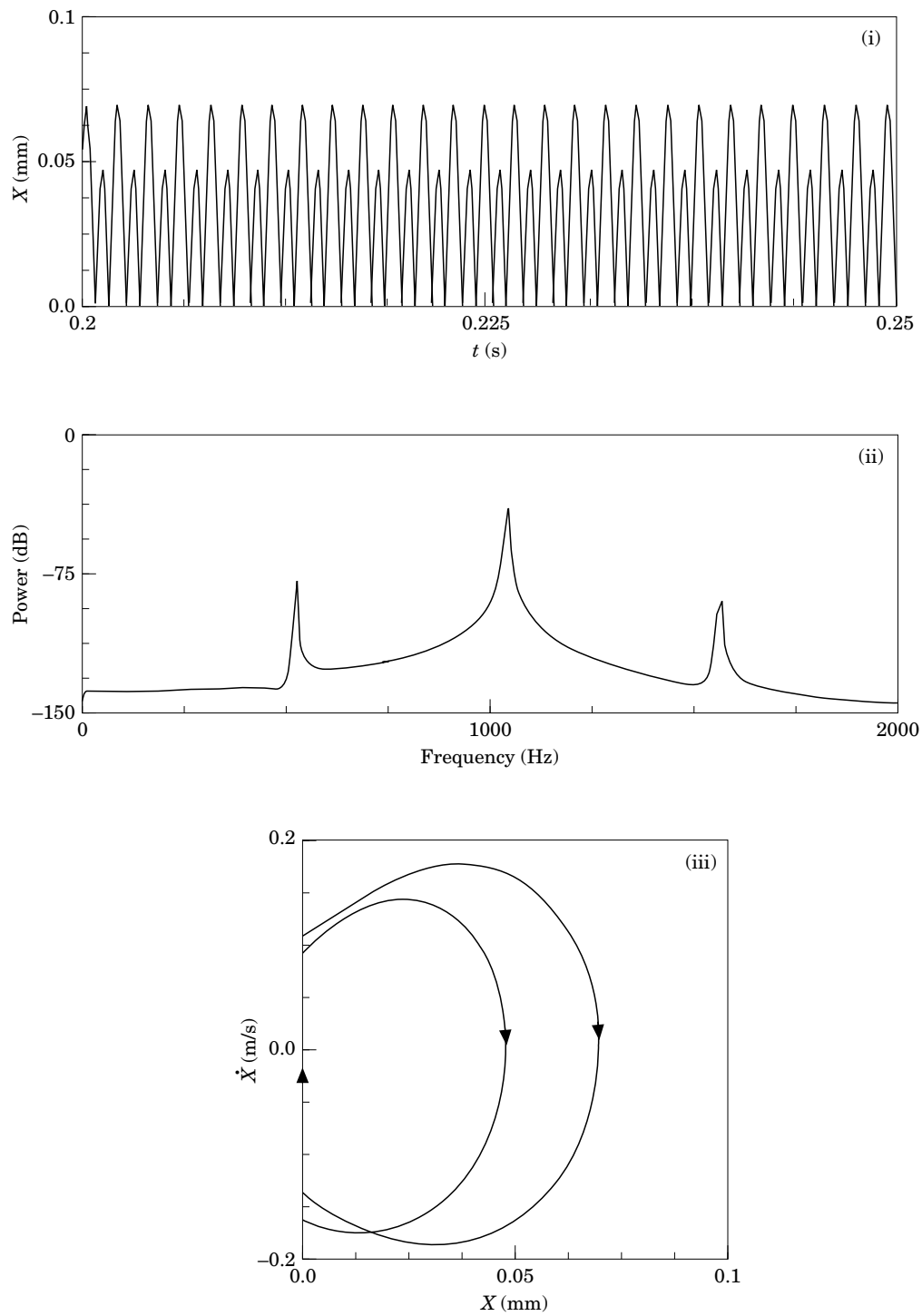


Figure 6(b). Comparison of self-excited vibrations in different supply pressure for  $P_s = 3.5$  MPa; period-two vibration. See key in Figure 6(a).

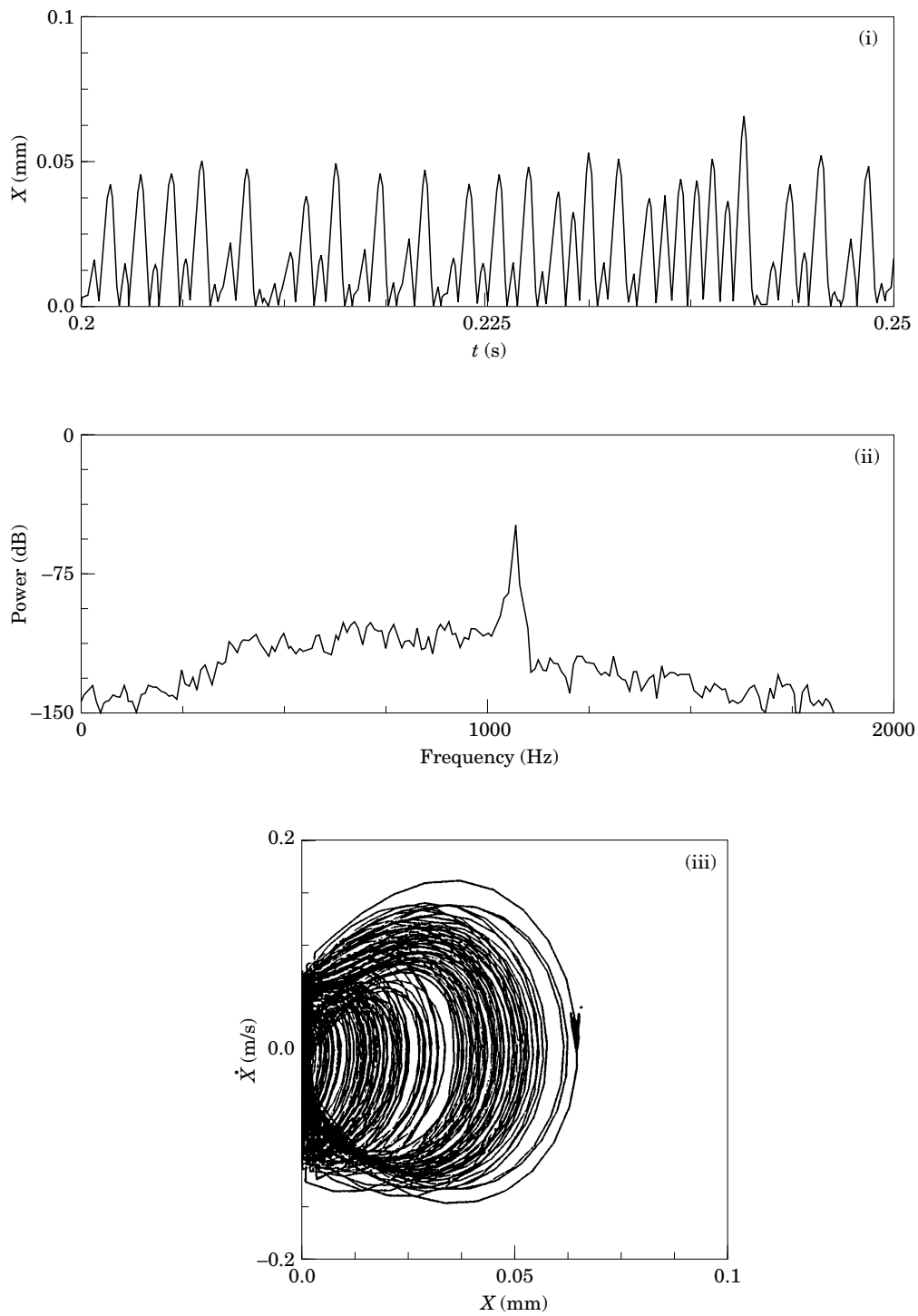


Figure 6(c). Comparison of self-excited vibrations in different supply pressure for  $P_s = 3.7$  MPa; chaotic vibration. See key in Figure 6(a).

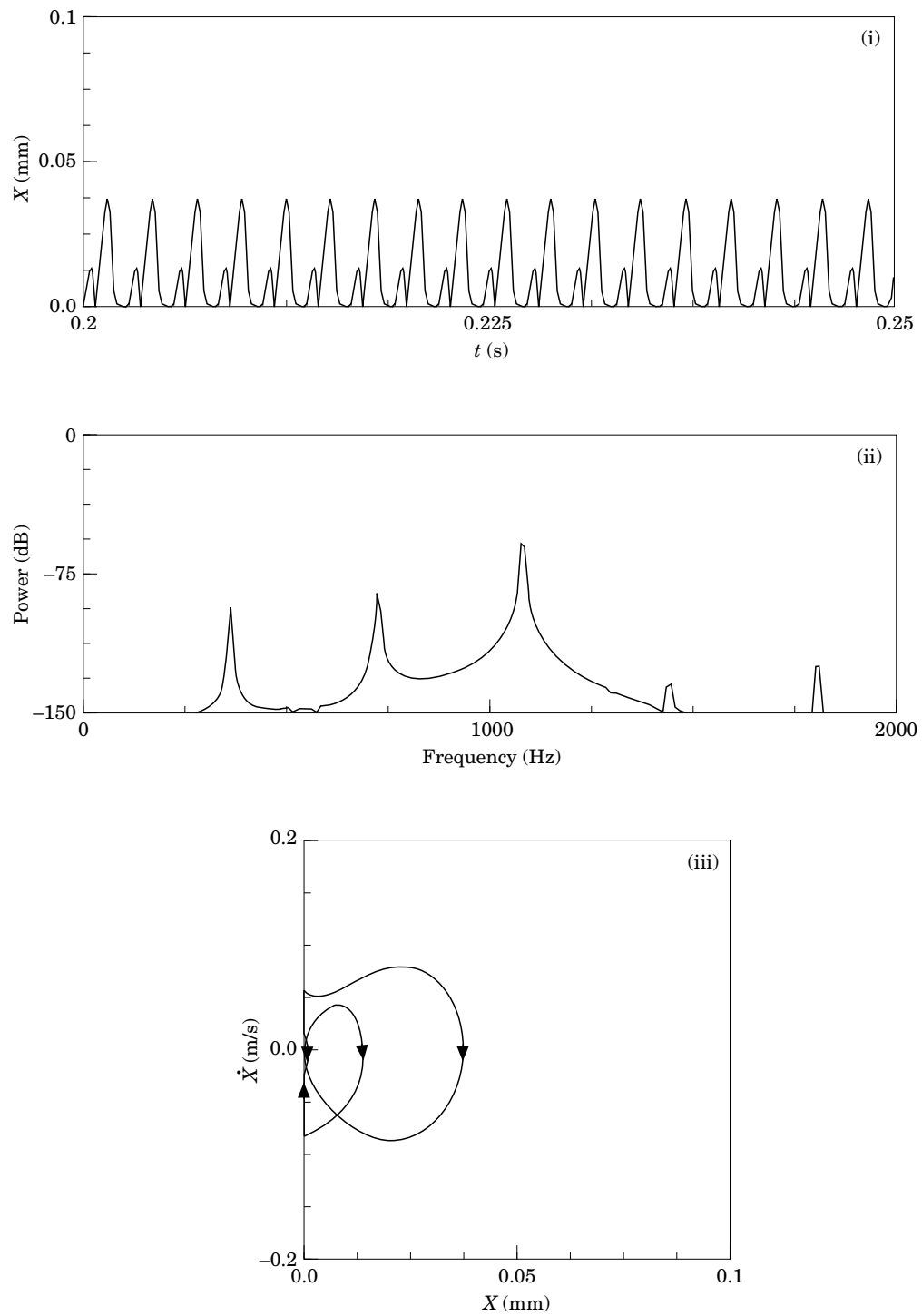


Figure 6(d). Comparison of self-excited vibrations in different supply pressure for  $P_s = 3.76$  MPa; period-three vibration. See key in Figure 6(a).

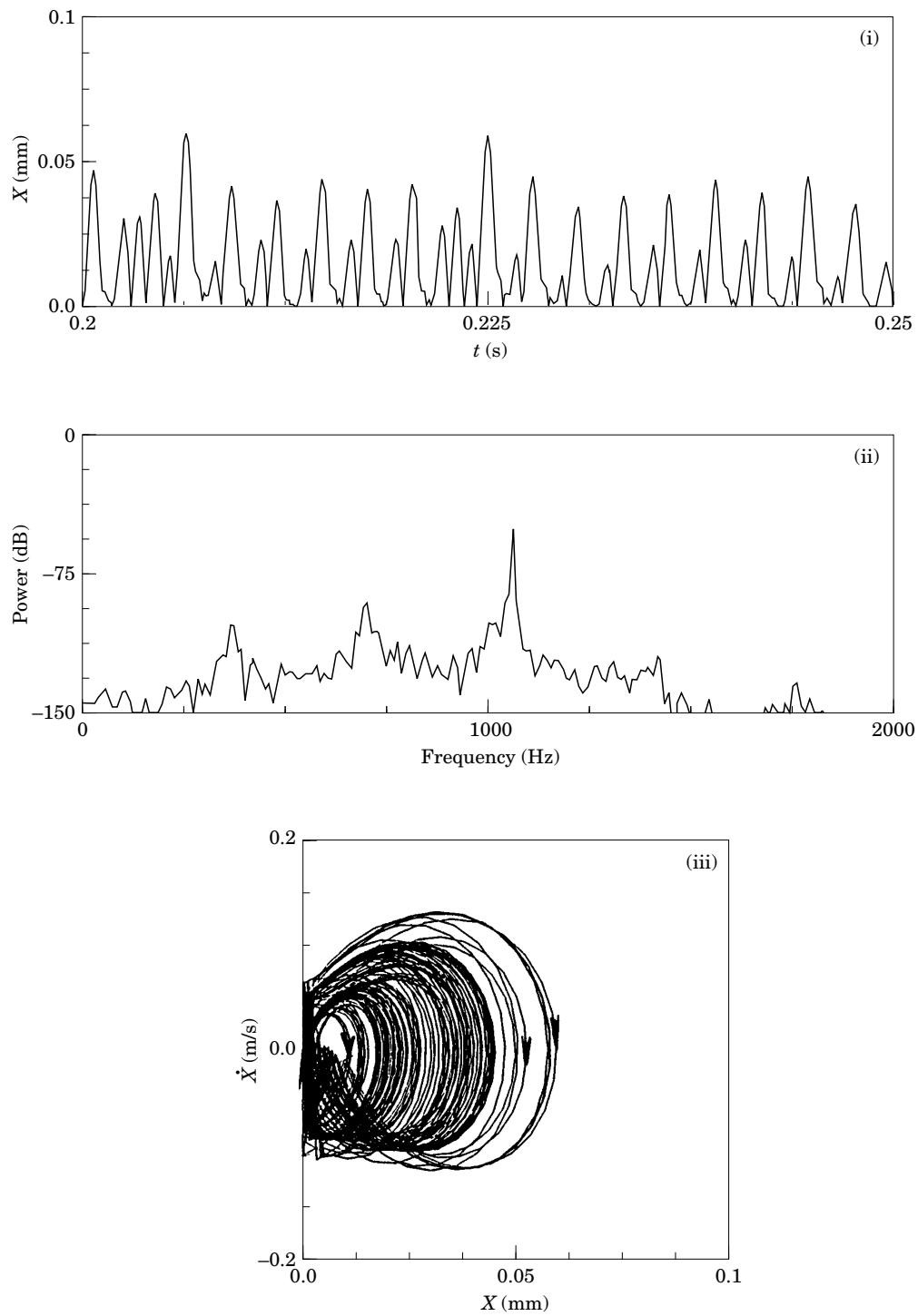


Figure 6(e). Comparison of self-excited vibrations in different supply pressure for  $P_s = 3.8$  MPa; chaotic vibration. See key in Figure 6(a).

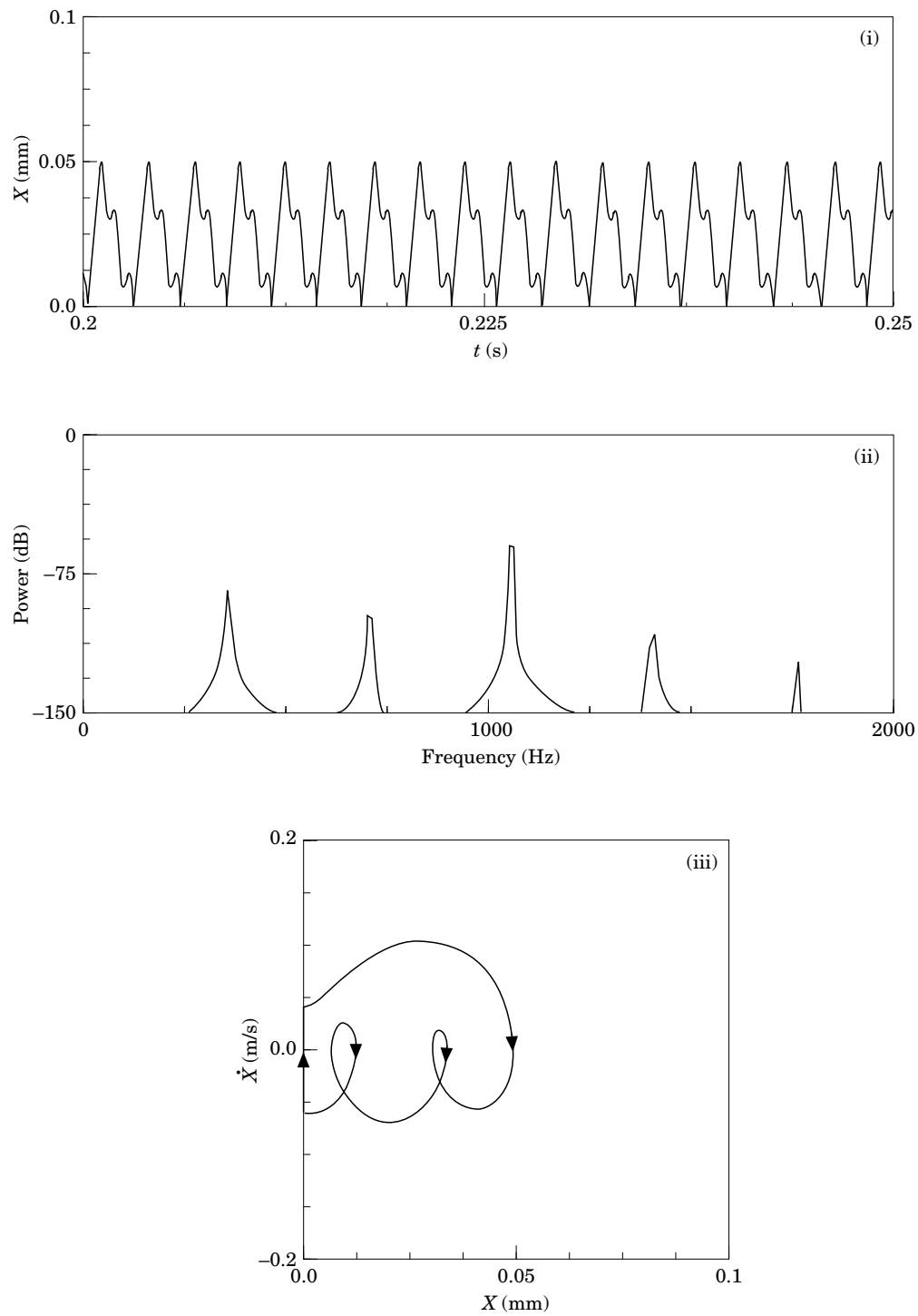


Figure 6(f). Comparison of self-excited vibrations in different supply pressure for  $P_s = 4.0$  MPa; period-three vibration. See key in Figure 6(a).



$P_s = 3.5$  MPa, the response bifurcates to period-2 vibration. In Figure 6(c), for  $P_s = 3.7$  MPa, the vibration is chaotic. The power spectrum rises at all frequencies, while the peak width broadens. These are typical features of chaotic phenomena. Increasing  $P_s$  still further, the vibration changes to period-3 and then becomes chaotic once again, as shown in Figure 6(d) for  $P_s = 3.76$  MPa and (e) for  $P_s = 3.8$  MPa. For higher  $P_s$ , the vibration passes through period-2 and period-3 [Figure 6(f)] vibrations and finally it returns to period-1, which is a conventional self-excited vibration.

#### 4.2. BIFURCATION DIAGRAM

Figure 7 is a bifurcation diagram on which all the maxima of the vibratory waves of the poppet displacement are plotted against supply pressure  $P_s$ . In this figure, the right-hand side dashed curve represents the static valve lift. The points A and B correspond to those in Figure 3; they indicate the stability boundary points. Other static points except the interval AB in the figure are locally stable as described previously.

The self-excited vibration undergoes a series of period-doubling bifurcations with increasing  $P_s$  leading to the first chaotic region. Figure 6(c) corresponds to the chaotic vibration occurring in this region. With further increase in  $P_s$ , a period-3 window corresponding to Figure 6(d) appears. At higher  $P_s$  still, the vibration enters the second chaotic regime. Figure 6(e) corresponds to the chaotic vibration occurring in this regime. The chaotic vibration disappears around  $P_s = 3.85$  MPa. The vibration goes through period-2 and period-3 and returns to period-1 vibration around the cracking pressure  $P_s = 4.0$  MPa.

The first period-doubling bifurcation sequence in Figure 7 is shown in detail in Figures 8(a), (b) and (c); Figures 8(b) and (c) are magnifications of the regions enclosed by squares in Figures 8(a) and (b), respectively. Bifurcation points obtained from the figures are listed in Table 2, where  $\mu_n$  represents the bifurcation point from the period- $2^{n-1}$  vibration to the period- $2^n$  vibration. Table 2 shows that the ratio  $\Delta_n = (\mu_{n-1} - \mu_{n-2}) / (\mu_n - \mu_{n-1})$  approaches the Feigenbaum number  $\Delta = \lim_{n \rightarrow \infty} \Delta_n = 4.6692016 \dots$  (Feigenbaum 1980). The bifurcation sequence resembles very much the Feigenbaum route to chaos.

Assuming that the ratio  $\Delta_n$  after  $n = 6$  can be approximated by the Feigenbaum number, the point of accumulation  $P_{\text{Sac}}$  is estimated from Table 2 as

$$\begin{aligned}
 P_{\text{Sac}} &= \mu_4 + (\mu_5 - \mu_4) + (\mu_6 - \mu_5) + (\mu_7 - \mu_6) + \dots \\
 &= \mu_4 + (\mu_5 - \mu_4) + (\mu_5 - \mu_4) \frac{1}{\Delta_6} + (\mu_5 - \mu_4) \frac{1}{\Delta_6 \Delta_7} + \dots \\
 &\approx \mu_4 + (\mu_5 - \mu_4) + (\mu_5 - \mu_4) \frac{1}{\Delta} + (\mu_5 - \mu_4) \frac{1}{\Delta^2} + \dots \\
 &\approx \mu_4 + (\mu_5 - \mu_4) \frac{1}{1 - \frac{1}{\Delta}} \approx 3.634852, \tag{18}
 \end{aligned}$$

where  $\mu_4 = 3.63409$ ,  $\mu_5 - \mu_4 = 0.000599$  and  $\Delta = 4.66920 \dots$ . The accumulation point is indicated in Figure 8.

## 4.3. LYAPUNOV EXPONENTS

Here we discuss the change of the largest Lyapunov exponent  $\lambda$  with supply pressure  $P_S$  used as the system parameter varied, by utilizing the method of Wolf *et al.* (1985) which makes use of time-series data of chaotic vibrations. The exponent  $\lambda$  is calculated as follows.

The state variables are defined as

$$Y = (X, \dot{X}, P_C, Q_O)^T, \quad (19)$$

and the governing equations are expressed as

$$\dot{Y} = F(Y). \quad (20)$$

A solution of equation (20) for an appropriate initial condition  $Y_0$  is taken as a fiducial

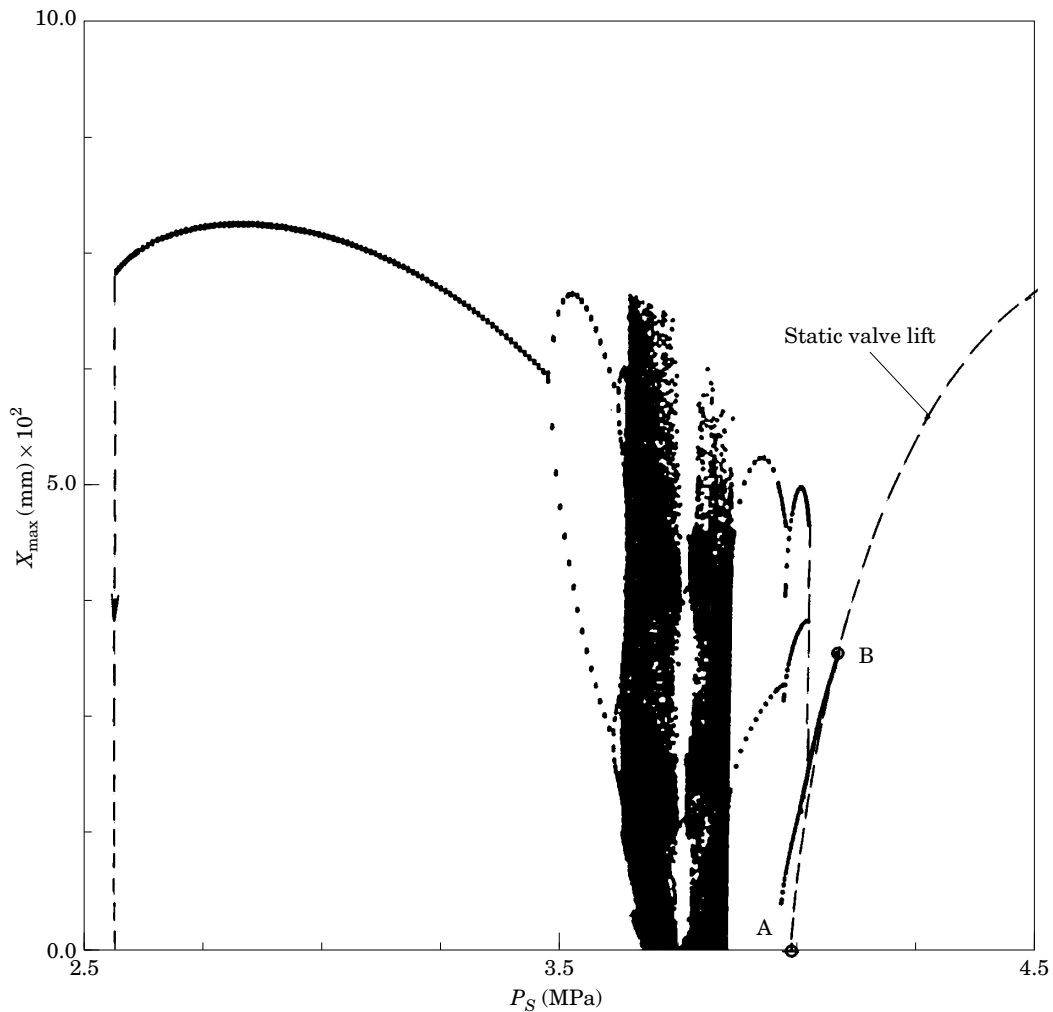


Figure 7. Bifurcation diagram of vibrations for operating point of  $P_{Si} = 4.0$  MPa.

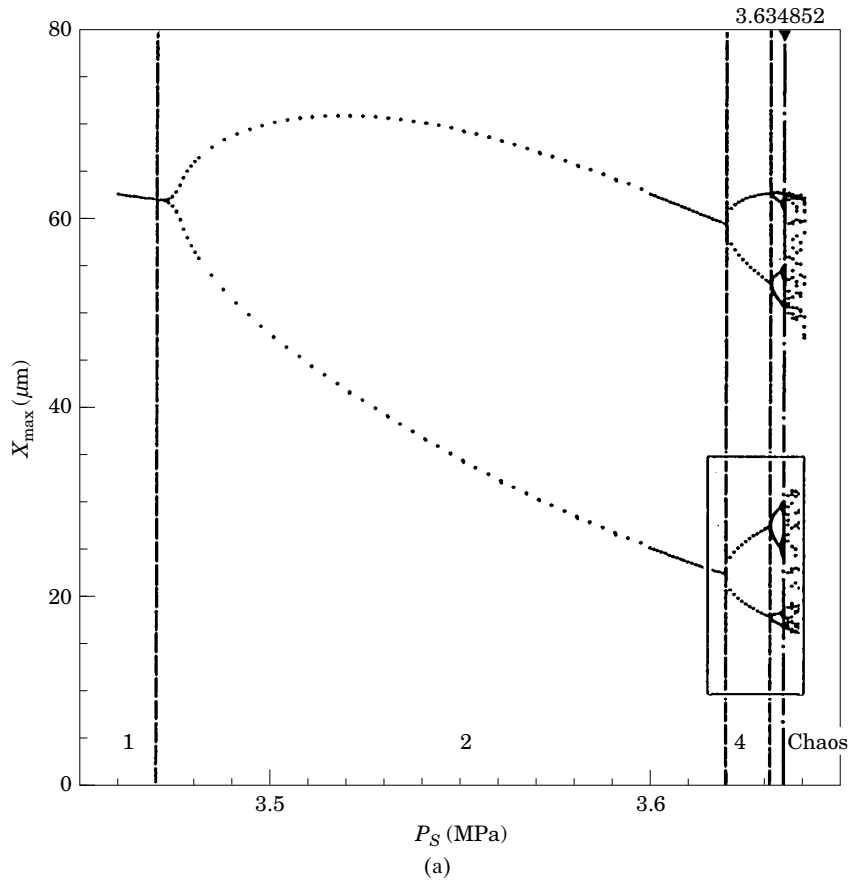


Figure 8. Enlargement of bifurcation map for period-doubling vibrations. (a) Bifurcation of  $1 \rightarrow 2 \rightarrow 4 \rightarrow 8$ ; (b) bifurcation of  $2 \rightarrow 4 \rightarrow 8 \rightarrow 16$ ; (c) bifurcation of  $8 \rightarrow 16 \rightarrow 32 \rightarrow 64$ .

solution, and let the state variable just after the  $n$ th collision at a certain time and the  $(n + 1)$ th collision be

$$Y_n = (0, \dot{X}_n^+, P_{Cn}, Q_{On})^T, \quad (21)$$

and

$$Y_{n+1} = (0, \dot{X}_{n+1}^+, P_{Cn+1}, Q_{On+1})^T, \quad (22)$$

respectively, where  $\dot{X}_n^+$ , and  $\dot{X}_{n+1}^+$  are the valve velocities just after the  $n$ th and  $(n + 1)$ th collisions.

Setting the time interval between successive  $n$ th and  $(n + 1)$ th collisions as  $\Delta t_n$ ,  $Y_{n+1}$  is calculated by the following integral for the initial condition  $Y_n$ :

$$Y_{n+1} = \int_0^{\Delta t_n} F(Y, Y_n) dt. \quad (23)$$

We consider the relation as a mapping from  $Y_n$  to  $Y_{n+1}$  which are discretized by successive collisions and represent the relation by

$$Y_{n+1} = f(Y_n). \quad (24)$$

By slightly shifting the initial condition from  $Y_n$  to  $Y_n + \delta Y_n$ , where  $\delta Y_n$  is a small

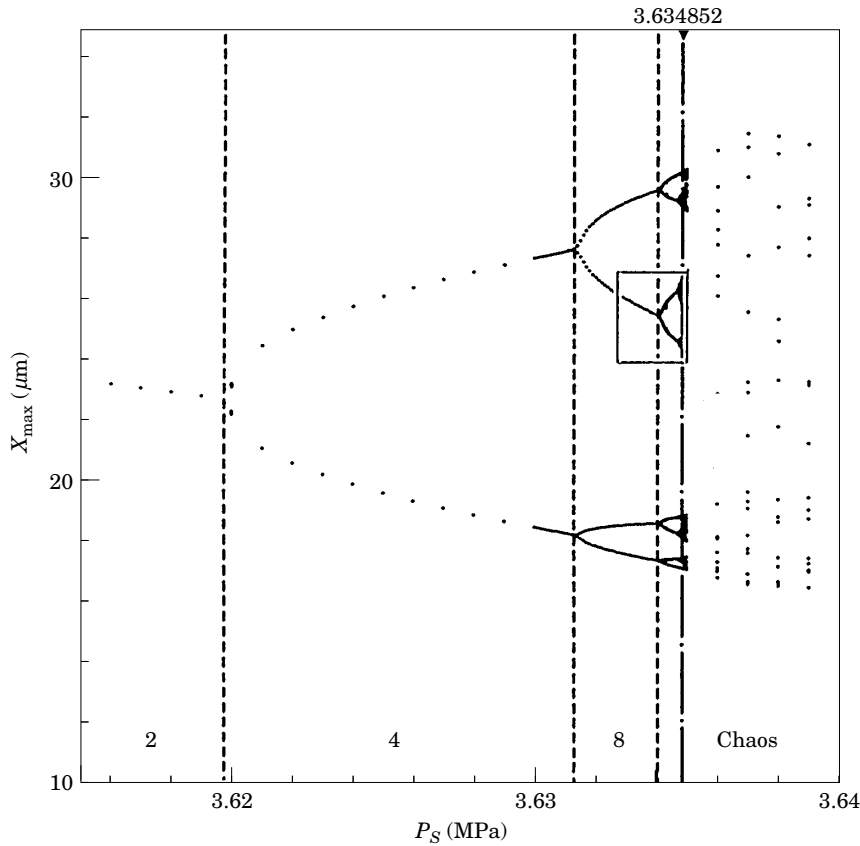


Figure 8. (Continued.)

perturbation whose direction coincides with  $Y_n$ , the state variable just after the successive collisions is given by

$$Y_{n+1} + \delta Y_{n+1} = \int_0^{\Delta t'_n} F(Y, Y_n + \delta Y_n) dt, \quad (25)$$

where  $\Delta t'_n$  means the time interval between the successive collisions for the slightly shifted infinitesimal conditions. From the above discussion, the Lyapunov exponent  $\lambda$  for the discrete dynamical system (24) can be approximated by

$$\begin{aligned} \lambda &= \lim_{N \rightarrow \infty} \frac{1}{N} \sum_{n=1}^{N-1} \log |f'(Y_n)| \\ &\approx \frac{1}{N} \sum_{n=1}^{N-1} \log \frac{|\delta Y_{n+1}|}{|\delta Y_n|}. \end{aligned} \quad (26)$$

In order to examine the influence of the magnitude of small perturbations  $|\delta Y_n|$  given as initial disturbances and of the iteration cycle  $N$  (the number of collisions) on convergence of the calculation for the Lyapunov exponent  $\lambda$ , the test calculations were carried out for  $|\delta Y_n| = 10^{-8}$ ,  $10^{-12}$ ,  $10^{-13}$  and the iteration cycle  $N = 1500$ . The operating condition of the system is chosen as  $P_{St} = 4.0$  MPa and  $P_S = 3.7$  MPa. The results are shown in Figure 9.

As seen in Figure 9, two curves plotted by a solid line and a dotted line with open

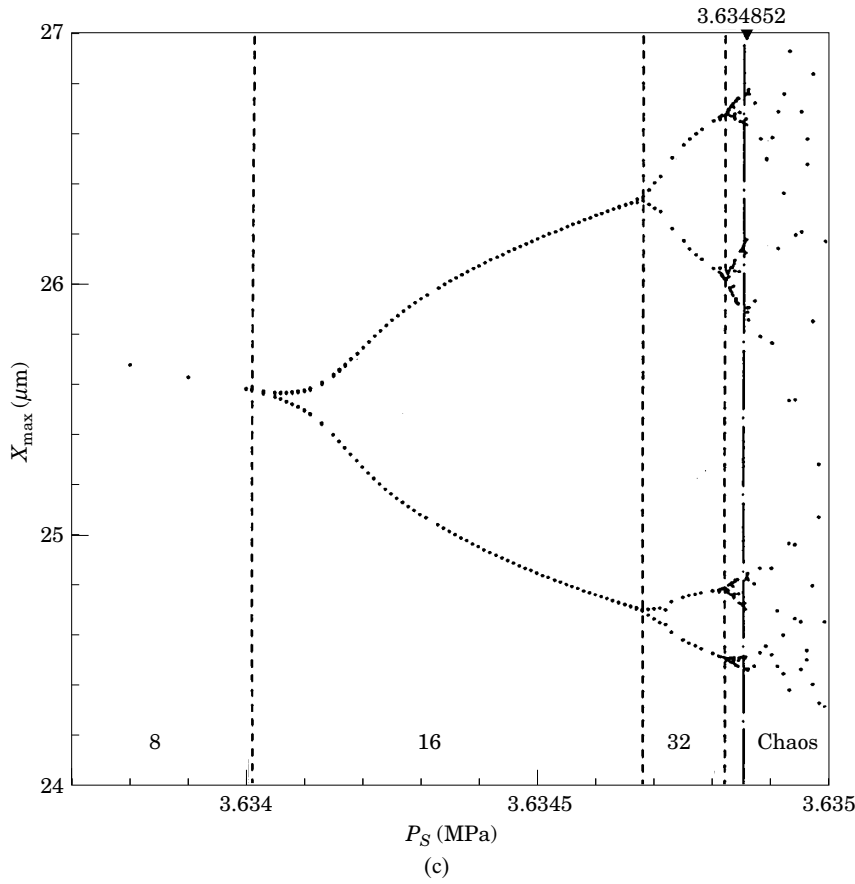


Figure 8. (Continued.)

circles (○) corresponding to  $|\delta Y_n| = 10^{-12}$  and  $10^{-8}$  converge to nearly the same value, and they do not show large changes for  $N > 500$ . On the other hand, the curve with closed circles (●) for the smallest perturbation  $|\delta Y_n| = 10^{-13}$  converges to a slightly different value from the other curves, and the variation for  $N > 500$  is somewhat larger than the others. This is considered to be caused by round-off errors; thus the calculation of  $\lambda$  was carried by using  $|\delta Y_n| = 10^{-12}$ .

Figure 10 shows the variation of  $\lambda$  with  $P_S$ . The positive region of  $\lambda$  coincides with the chaotic region in Figure 7, where points are densely distributed. In the region for the

TABLE 2  
Bifurcation sequences

$n$	$2^{n-1} \rightarrow 2^n$	$\mu_n$	$\mu_n - \mu_{n-1}$	$\Delta_n$
1	1 → 2	3.47000	—	—
2	2 → 4	3.61974	0.14972	—
3	4 → 8	3.631291	0.01155	12.963
4	8 → 16	3.634090	0.00280	4.125
5	16 → 32	3.634689	0.000599	4.674
6	32 → 64	3.634820	0.000131	4.573

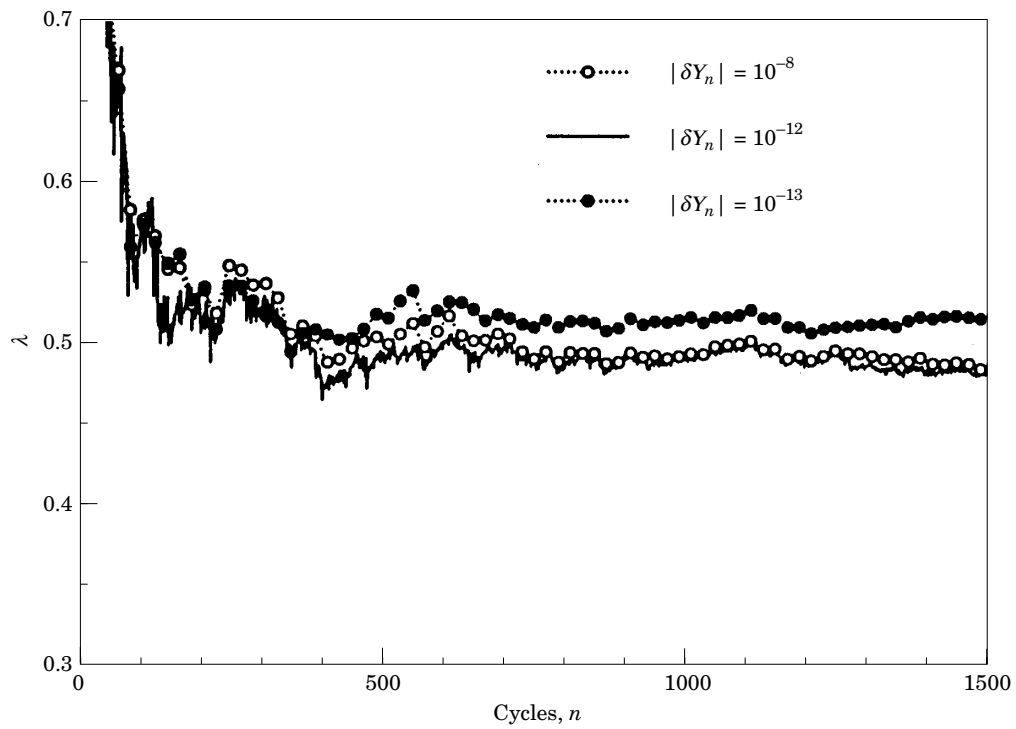


Figure 9. Convergence of Lyapunov exponent with cycle number  $n$ . (○)  $\delta Y_n = 10^{-8}$ ; (—)  $\delta Y_n = 10^{-12}$ ; (●)  $\delta Y_n = 10^{-13}$ .

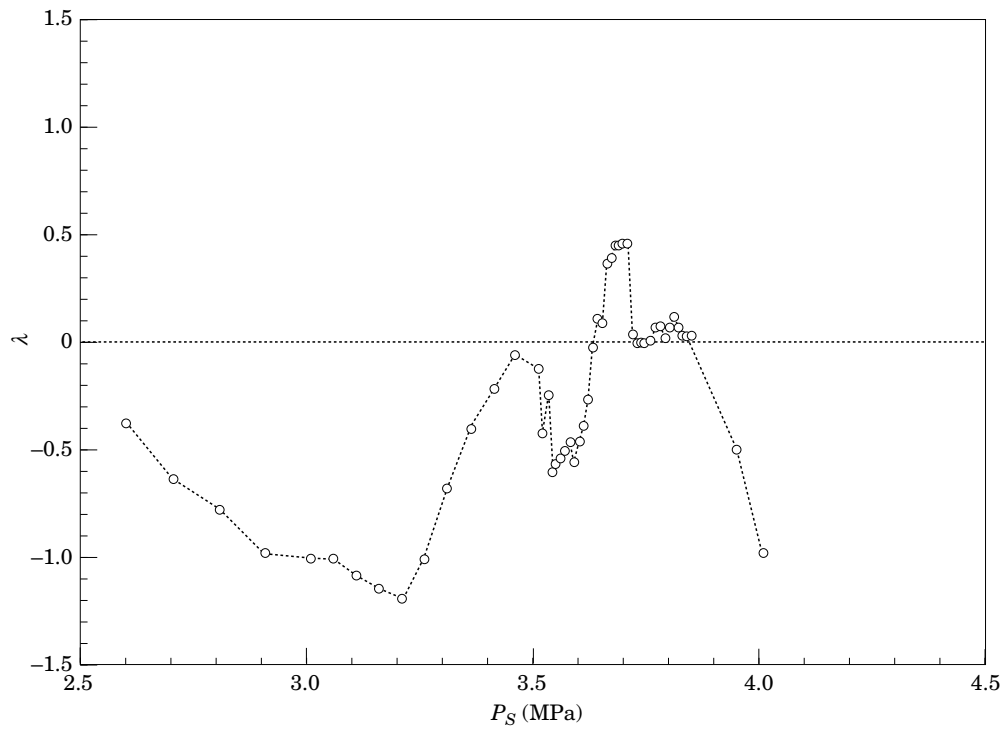


Figure 10. Lyapunov exponent with supply pressure ( $P_{Si} = 4.0$  MPa).

window of period-3 vibration,  $\lambda$  does not become negative, but it becomes nearly zero in this calculation.

## 5. CONCLUSIONS

We have numerically studied chaotic vibratory phenomena in a poppet valve circuit with a relatively short supply line by means of power spectra, a bifurcation diagram and Lyapunov exponents. It is clarified that the predominant dynamics are a period-doubling sequence culminating in chaos, followed by a reversal to period-1 motion at high values of the supply pressure, which is the system parameter varied. The period-doubling route to chaos is quantitatively confirmed by computation of the associated universal Feigenbaum number. Calculations of the largest positive Lyapunov exponent confirms the existence of chaos. This dynamical behaviour occurs for supply pressures lower than the cracking pressure of the poppet valve.

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## APPENDIX: NOMENCLATURE

$A_L$	cross-sectional area of pipeline, $\pi d_L^2/4$
$A_O$	opening area of orifice, $\pi d_O^2/4$
$A_P$	cross-sectional area of valve seat, $\pi d_P^2/4$
$a_P$	equivalent cross-sectional area of valve seat, $[\partial F/\partial P_C]_E$
$C$	capacitance of valve chamber, $V/\beta$
$C_O$	discharge coefficient of orifice
$C_P$	discharge coefficient of poppet valve
$C_{P0}$	discharge coefficient of poppet valve for large valve lift
$c_P$	linearized discharge coefficient of poppet valve $[\partial Q_C/\partial P_C]_E$
$c_X$	linearized flow gain of poppet valve, $[\partial Q_C/\partial X]_E$
$d_L$	inner diameter of pipeline
$d_O$	diameter of orifice aperture
$d_P$	diameter of poppet valve seat aperture
$e$	restitution coefficient of poppet to valve seat
$F$	axial flow force acting on poppet
$f_0$	initial compression force of suspension spring, $kX_i$
$h$	time stepsize in Runge–Kutta computation
$I$	inertance of pipeline, $\rho L/A_L$
$k$	spring constant of suspension spring
$k_X$	hydraulic spring force, $[\partial F/\partial X]_E$
$L$	supply pipeline length
$m$	poppet mass
$P_C$	pressure in valve chamber
$P_{CE}$	static valve chamber pressure
$P_O$	upstream pressure of orifice
$P_S$	supply pressure
$P_{Si}$	cracking pressure, $f_0/A_P$
$p_C$	variational valve chamber pressure
$Q_{OE}$	static flow
$Q_O$	flow rate through orifice
$Q_C$	flow rate through poppet valve
$q_O$	variational flow rate through orifice
$V$	volume of poppet chamber
$X$	poppet valve displacement (valve lift)
$X_E$	static valve lift
$X_i$	initially compressed length of suspension spring
$X_{ref}$	reference quantity for valve lift
$x$	variational displacement of poppet valve
$\Delta$	Feigenbaum number
$\alpha$	half angle of poppet
$\beta$	bulk modulus of working fluid (oil)
$\gamma$	poppet valve factor
$\delta$	viscous damping coefficient
$\lambda$	Lyapunov exponent
$\mu_n$	bifurcation point
$\rho$	density of working fluid